

## AMENDMENTS TO THE SPECIFICATION

Please insert the following new section and headings between paragraphs [0059] and [0060] of the specification:

### BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a simplified flow diagram of a process for selectively removing sulphur compounds from synthesis gas, in accordance with an embodiment of the present invention;

Fig. 2 is a graph illustrating the relationship between temperature and reduction of basic carbonates in the flow diagram of Fig. 1;

Fig. 3 is a graph illustrating the outlet concentration of  $\text{H}_2\text{S}$  and  $\text{COS}$  as a function of time; and

Fig. 4 is a graph illustrating the outlet concentration of  $\text{H}_2\text{S}$  and  $\text{COS}$  as a function of time and in the presence of  $\text{Cu/ZnO/Al}_2\text{O}_3$ .

### DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

Please amend the line spacing of the footnotes of TABLE 1 as follows:

\* The equilibrium conversions to CH<sub>3</sub>OH for Syngas B is calculated on the basis that the activation of CO does not take place on the catalyst:  $2\text{H}_2 + \text{CO} \rightarrow \text{CH}_3\text{OH}$ , as shown by Rozovskii.

\*\* Equilibrated gas contains 11 ppm of CO, build by reverse shift. The building of 11 ppm is far below the critical limit of the formation level of 1000 ppm of components not contained in the feed gas.

\*\*\* CO is converted into methanol via the water gas shift reaction as water is present in the feed.